

FORM PTO-1390 (REV. 9-2001)		U.S. DEPARTMENT OF COMMERCE PATENT AND TRADEMARK OFFICE		ATTORNEY'S DOCKET NUMBER 366325-520
<b>TRANSMITTAL LETTER TO THE UNITED STATES DESIGNATED/ELECTED OFFICE (DO/EO/US) CONCERNING A FILING UNDER 35 U.S.C. 371</b>				U.S. APPLICATION NO. (If known, see 37 CFR 1.5) <b>10/009718</b> Not yet assigned
INTERNATIONAL APPLICATION NO. PCT/FR00/01669	INTERNATIONAL FILING DATE 16 June 2000 (16.06.2000)	PRIORITY DATE CLAIMED 18 June 1999 (18.6.1999)		
<b>TITLE OF INVENTION</b> Method for Fractionating Cooking Oil				
<b>APPLICANT(S) FOR DO/EO/US</b> Perrut, et al.				
Applicant herewith submits to the United States Designated/Elected Office (DO/EO/US) the following items and other information:				
<ol style="list-style-type: none"> <li>1. <input checked="" type="checkbox"/> This is a <b>FIRST</b> submission of items concerning a filing under 35 U.S.C. 371.</li> <li>2. <input type="checkbox"/> This is a <b>SECOND</b> or <b>SUBSEQUENT</b> submission of items concerning a filing under 35 U.S.C. 371.</li> <li>3. <input checked="" type="checkbox"/> This is an express request to begin national examination procedures (35 U.S.C. 371(f)). The submission must include items (5), (6), (9) and (21) indicated below.</li> <li>4. <input type="checkbox"/> The US has been elected by the expiration of 19 months from the priority date (Article 31).</li> <li>5. <input checked="" type="checkbox"/> A copy of the International Application as filed (35 U.S.C. 371(c)(2))             <ol style="list-style-type: none"> <li>a. <input checked="" type="checkbox"/> is attached hereto (required only if not communicated by the International Bureau).</li> <li>b. <input type="checkbox"/> has been communicated by the International Bureau.</li> <li>c. <input type="checkbox"/> is not required, as the application was filed in the United States Receiving Office (RO/US).</li> </ol> </li> <li>6. <input checked="" type="checkbox"/> An English language translation of the International Application as filed (35 U.S.C. 371(c)(2)).             <ol style="list-style-type: none"> <li>a. <input checked="" type="checkbox"/> is attached hereto.</li> <li>b. <input type="checkbox"/> has been previously submitted under 35 U.S.C. 154(d)(4).</li> </ol> </li> <li>7. <input type="checkbox"/> Amendments to the claims of the International Application under PCT Article 19 (35 U.S.C. 371(c)(3))             <ol style="list-style-type: none"> <li>a. <input type="checkbox"/> are attached hereto (required only if not communicated by the International Bureau).</li> <li>b. <input type="checkbox"/> have been communicated by the International Bureau.</li> <li>c. <input type="checkbox"/> have not been made; however, the time limit for making such amendments has NOT expired.</li> <li>d. <input type="checkbox"/> have not been made and will not be made.</li> </ol> </li> <li>8. <input type="checkbox"/> An English language translation of the amendments to the claims under PCT Article 19 (35 U.S.C. 371(c)(3)).</li> <li>9. <input checked="" type="checkbox"/> An oath or declaration of the inventor(s) (35 U.S.C. 371(c)(4)).</li> <li>10. <input type="checkbox"/> An English language translation of the annexes of the International Preliminary Examination Report under PCT Article 36 (35 U.S.C. 371(c)(5)).</li> </ol>				
<b>Items 11 to 20 below concern document(s) or information included:</b> <ol style="list-style-type: none"> <li>11. <input type="checkbox"/> An Information Disclosure Statement under 37 CFR 1.97 and 1.98.</li> <li>12. <input type="checkbox"/> An assignment document for recording. A separate cover sheet in compliance with 37 CFR 3.28 and 3.31 is included.</li> <li>13. <input type="checkbox"/> A <b>FIRST</b> preliminary amendment.</li> <li>14. <input type="checkbox"/> A <b>SECOND</b> or <b>SUBSEQUENT</b> preliminary amendment.</li> <li>15. <input type="checkbox"/> A substitute specification.</li> <li>16. <input checked="" type="checkbox"/> A change of power of attorney and/or address letter.</li> <li>17. <input type="checkbox"/> A computer-readable form of the sequence listing in accordance with PCT Rule 13ter.2 and 35 U.S.C. 1.821 - 1.825.</li> <li>18. <input type="checkbox"/> A second copy of the published international application under 35 U.S.C. 154(d)(4).</li> <li>19. <input type="checkbox"/> A second copy of the English language translation of the international application under 35 U.S.C. 154(d)(4).</li> <li>20. <input type="checkbox"/> Other items or information:</li> </ol>				

U.S. APPLICATION NO. OR known sec 37 CFR 1.5  
107009718  
Not yet assignedINTERNATIONAL APPLICATION NO  
PCT/FR00/01669ATTORNEY'S DOCKET NUMBER  
366325-52021.  The following fees are submitted:**BASIC NATIONAL FEE (37 CFR 1.492 (a) (1) - (5)):**

Neither international preliminary examination fee (37 CFR 1.482) nor international search fee (37 CFR 1.445(a)(2)) paid to USPTO and International Search Report not prepared by the EPO or JPO ..... \$1040.00

International preliminary examination fee (37 CFR 1.482) not paid to USPTO but International Search Report prepared by the EPO or JPO ..... \$890.00

International preliminary examination fee (37 CFR 1.482) not paid to USPTO but international search fee (37 CFR 1.445(a)(2)) paid to USPTO ..... \$740.00

International preliminary examination fee (37 CFR 1.482) paid to USPTO but all claims did not satisfy provisions of PCT Article 33(1)-(4) ..... \$710.00

International preliminary examination fee (37 CFR 1.482) paid to USPTO and all claims satisfied provisions of PCT Article 33(1)-(4) ..... \$100.00

**ENTER APPROPRIATE BASIC FEE AMOUNT =****CALCULATIONS PTO USE ONLY**

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CLAIMS				RATE
Total claims 14 - 20 = --				x \$18.00 \$ 0.00
Independent claims 1 - 3 = 0				x \$84.00 \$ 0.00
MULTIPLE DEPENDENT CLAIM(S) (if applicable)				+ \$282.00 \$ 282.00
<b>TOTAL OF ABOVE CALCULATIONS =</b>				\$ 1,172.00
<input type="checkbox"/> Applicant claims small entity status. See 37 CFR 1.27. The fees indicated above are reduced by 1/2.				+ \$ 0.00
<b>SUBTOTAL =</b>				\$ 1,172.00
Processing fee of \$130.00 for furnishing the English translation later than <input type="checkbox"/> 20 <input type="checkbox"/> 30 months from the earliest claimed priority date (37 CFR 1.492(f)).				\$ 0.00
<b>TOTAL NATIONAL FEE =</b>				\$ 1,172.00
Fee for recording the enclosed assignment (37 CFR 1.21(h)). The assignment must be accompanied by an appropriate cover sheet (37 CFR 3.28, 3.31). \$40.00 per property +				\$ 0.00
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				<b>Amount to be refunded:</b> \$
				<b>charged:</b> \$

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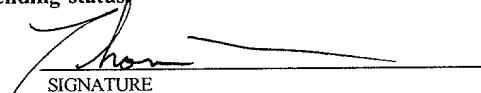
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**NOTE: Where an appropriate time limit under 37 CFR 1.494 or 1.495 has not been met, a petition to revive (37 CFR 1.137 (a) or (b)) must be filed and granted to restore the application to pending status**

SEND ALL CORRESPONDENCE TO:

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REGISTRATION NUMBER

METHOD FOR FRACTIONATING COOKING OIL

The present invention relates to an industrial method for fractionating mixtures of lipids with the aid of a solvent taken to supercritical pressure, i.e. a fluid in supercritical state or a subcritical liquid, with a view to obtaining, from used cooking oils, a refined oil, decoloured and deodorized, from which are removed products of oxidation and other products of degradation formed during use of these oils.

The consumption of fried food, particularly fried potatoes, has considerably increased in the majority of developed countries, with the development of new types of restauration and new industrially cooked foods. This has logically led to a considerable increase in the production of used frying oils. The latter represent a considerable volume of waste, amounting to hundreds of thousands of tons per year in Europe, constituting a very serious potential threat of pollution of surface water. As at the present time it cannot be envisaged to re-use them, they are generally destroyed by incineration and only their calorific power is possibly recuperated.

The present invention has for its object to propose a method for industrially treating these used cooking oils in order to obtain a refined oil capable of being used as food component for animals, particularly for poultry.

This refined oil must therefore be bereft of products likely to be detrimental to the health of the animals thus

fed, and must, in addition, be obtained at a cost compatible with an industrial exploitation. Of course, this refined oil must not represent risks for the consumer of the meat of the animals thus fed either, or add unpleasant tastes to this meat. It is therefore essential to eliminate the products of degradation of the oil which are formed during cooking and in particular those which give the oil a dark, even black colour and a highly sickening characteristic odour, which characterize for example frying oils after prolonged use.

The method according to the invention will call upon a method of separation employing a fluid at supercritical pressure.

In effect, it is known that bodies are generally known in three states: solid, liquid and gaseous. One passes from one to the other by varying the temperature and/or the pressure. Now, there is a point beyond which one can pass from the liquid state to the vapour state without passing through a boiling, or, inversely, by a condensation, but continuously: this point is called the critical point.

Under these conditions, a fluid in a supercritical state is a fluid which is in a state characterized either by a pressure and temperature respectively higher than the critical pressure and temperature in the case of a pure body, or by a representative point (pressure, temperature) located beyond the envelope of the critical points represented on a diagram (pressure, temperature) in the case of a mixture. Such a fluid presents, for very numerous substances, a

high solvent power incomparable to that observed for this same fluid when it is in the state of compressed gas. The same applies to so-called "sub-critical" liquids, i.e. which are in a state characterized either by a pressure higher than the critical pressure and by a temperature lower than the critical temperature in the case of a  
5 pure body, or by a pressure higher than the critical pressures and a temperature lower than the critical temperatures of the components in the case of a mixture.

The considerable and modulatable variations of the solvent power of these fluids are, moreover, used in numerous methods of extraction (solid/fluid), of fractionation (liquid/fluid), of analytic or preparative chromatography, of  
10 treatment of materials (ceramics, polymers). Chemical or biochemical reactions are also made in such solvents.

Among the different solvents which may be used under a supercritical pressure, carbon dioxide is particularly interesting due to its critical pressure of 7.4 MPa and its critical temperature of 31°C, which make of it a preferred solvent  
15 in numerous applications, all the more so as it does not present any toxicity and it is available in very large quantities at very low cost. As non-polar solvent, carbon dioxide taken to supercritical pressure sometimes has a co-solvent added thereto, constituted by a polar organic solvent which modifies the solvent power in noteworthy manner

especially with respect to molecules presenting a certain polarity, ethanol often being used to that end.

One of the principal advantages of the methods in which a fluid at supercritical pressure is used as solvent resides in the ease of effecting separation between the solvent and the extracts and solutes collected, as has been described in numerous publications and, for certain important aspects of implementation, in French Patent FR-A-2 584 618. The interesting properties of these fluids are moreover used in solid-fluid extraction and liquid-fluid fractionation, as is described in the afore-mentioned document.

Fractionation of the lipids by a fluid at supercritical pressure has been described in the prior state of the art, and reference may be made to a recent work "Supercritical Fluid technology in Oil and Lipid Chemistry" edited by J.W. KING and G.R. LIST. For example, pure carbon dioxide has been used as solvent of glycerides in order to extract the oils of different natural sources such as oleaginous seeds. The operations of fractionating lipids with the aid of solvents at supercritical pressure often encounter serious difficulties in implementation, as the initial or resultant phases are often very pasty, which renders contact with the solvent fluid difficult and even impossible to effect. Certain devices for dealing with this problem have been described, such as for example a jet extractor system proposed by EGGER E., WAGNER H., ("Proceedings of the Third International Symposium on Supercritical Fluids")

in order to remove oil from a soja lecithin. However, this system comprises at the most only one theoretical stage and it is thus not possible to effect a fractionation of very similar compounds requiring a high number of theoretical plateaux generally employed on multi-staged columns with perforated plateaux or lining functioning in counter-current. This method proves to be high-performance; however, although it is well adapted to the treatment of high-quality oils of high price intended for dietetics or pharmacy, its cost price is often too high to ensure industrial purification of wastes such as cooking oils.

Another method of fractionating lipids has also been proposed, described in particular in US Patent US-A-5 759 549, in which the mixture to be fractionated is adsorbed on a porous solid, from which the different components are successively extracted by a fluid at supercritical pressure whose solvent power and polarity are successively increased. This method, of which the concept has been used for several years, is known under the name of "extrography". It will be noted that this method may be carried out with a high selectivity, by combination of the selectivity of the adsorbent solid and of that of the solvent at supercritical pressure, but requires complex means and can be carried out only in batch mode, which involves very high operating costs.

The object of the present invention is to propose a method making it possible, for industrial production purposes, to effect fractionation of used cooking oils

with a view to obtaining a refined oil and a residue representing a limited volume with respect to the feedstock, with the aid of a solvent taken to supercritical pressure, by using a very simple installation and inexpensive to carry out.

The present invention thus has for its object a method for fractionating a  
5 cooking oil, in particular frying oil, using a solvent at supercritical pressure,  
characterized in that it comprises the steps consisting in:

- contacting, in a mixer, the cooking oil with the solvent at supercritical pressure;
- separating the resulting mixture into two phases in a decanter, namely a  
10 light phase and heavy phase;
- decompressing the light phase and the heavy phase so as to recuperate the solvent and the treated oil and the treatment residues respectively.

According to the invention, this fractionation is effected on an equipment consisting of an assembly of "mixer-decanter" type constituted by a mixer within  
15 which the oil to be treated and the solvent at supercritical pressure are intimately mixed, and by a decanter maintained at a pressure less than or equal to that prevailing in the mixer, within which the diphasic mixture thus produced is separated into its two phases, namely the heavy phase constituted by the non-extracted oil residue and a low concentration of solvent at supercritical pressure  
20 which is dissolved therein, and the light phase, constituted by the fluid

at supercritical pressure and the components of the oil which are dissolved therein.

The heavy phase is advantageously recycled, partly in the mixer and partly decompressed to atmospheric pressure and constitutes the residue which is very  
5 dark with an unpleasant odour.

In an embodiment of the invention, the fluid at supercritical pressure is constituted by a mixture of an organic solvent in carbon dioxide. In this case, a small quantity of this organic solvent is still present in the residue after decompression of the heavy phase and will be separated, in a conventional  
10 evaporator for example, in order that the residue can be more easily manipulated and possibly destroyed, and that the organic solvent thus recuperated can be recycled. Such an organic solvent may be constituted in particular by a light hydrocarbon having between 2 and 5 carbon atoms, such as ethane, propane and butane. The operating pressure will be included between 7.4 PMa and 50 Mpa  
15 and more favourably between 20 MPa and 40 MPa, the temperature itself being included between 0°C and 80°C. Such a solvent may also be constituted by an alcohol, such as in particular ethanol, or by a ketone, such as in particular acetone, or by an ester, such as in particular ethyl acetate.

The light phase is decompressed in order to effect separation of the solvent  
20 from the treated oil which constitutes the extract. It will be recalled that the prior state of the art proposes means for optimalizing the separation between the solvent and the extract, in particular

thanks to the devices described in afore-mentioned French Patent FR-A-2 584 618. The extracted oil is thus bereft of the products of degradation resulting from the use of the initial oil as frying medium, in particular of those which give it a dark, even black colour and a highly sickening characteristic odour.

5 A form of embodiment of the present invention will be described hereinafter by way of non-limiting example, with reference to the accompanying drawing in which the single Figure schematically shows an installation for carrying out the method according to the invention.

This installation essentially comprises a mixer 1 of which the outlet A  
10 supplies a separator 3. The mixer 1 is constituted by a cylindrical recipient with a diameter of 58 mm and a height of 1 m which is filled with a lining of stainless steel of "Intalox" type 10 mm thick and which is provided with a double-jacket allowing the circulation of a heat-transfer fluid. The inlet B of the mixer 1 is connected to a volumetric diaphragm pump 5 which supplies the latter with  
15 cooking oil to be purified, after the latter has been taken to a sufficient temperature to give it a fluidity allowing it to be pumped. The inlet B of the mixer 1 is also connected to an exchanger 7 which is itself connected to two pumps, namely a volumetric diaphragm pump 9 which delivers the solvent, in the present case carbon dioxide, and a pump 11 of the same type which supplies a co-  
20 solvent, in the present case ethanol, which is contained in a tank 13. The pump 9 compresses the carbon dioxide to its supercritical pressure,

and the exchanger 7 ensures heating of the solvent and the co-solvent. After mixture, the fluid admitted into the separator 3 is decanted therein and is maintained at a pressure close to or slightly less than that prevailing in the mixer 1.

5       The raffinate emerges at R at the foot of the separator 3, and is decompressed to the pressure of recycling of the fluid, viz. about 4.5 MPa, in a recipient 15 within which expansion takes place, at a pressure less than that prevailing in the separator 3, which allows degassing of the liquid and the partial recycling of the vaporized solvent. The solvent laden with extract emerges at the  
10 head S of the separator 3, and is decompressed via a valve 17 of discharge type. The drop in pressure brings about separation of the mixture which is admitted into an assembly of separators 19, 21, 23 constituted, in accordance with the system described in afore-mentioned French Patent FR-A-2 584 618, by cyclone chambers allowing the total separation of the liquid phase and the gaseous phase  
15 with addition of heat via the walls of the separators of which the double-jacket has hot water passing therethrough, which makes it possible to bring the enthalpy required to ensure vaporization of the solvent.

The liquid phase collected in the separators 19, 21, 23 is drawn off, at atmospheric pressure, via a system of lock chambers 25, 27, 29 respectively. The  
20 solvent from which the extract and part of the co-solvent has been removed is liquefied in a double-tube condenser 31 of which the outer tube has passing therethrough a mixture of water-ethylene glycol cooled towards 0°C, stored in the liquid state at about 5°C in a tank 33 of which the level is maintained stable by an

addition of carbon dioxide from an outside tank and which is connected to pump 9.

As the method requires a high flowrate of oil in order to improve the contact between the oil and the fluid at supercritical pressure, it will be noted that 5 it is useful to recycle part of the raffinate in the feedstock in order to increase the yield of extraction in valorizable compounds.

EXAMPLE 1: Treatment of a used frying oil in a mixer-decanter:

In such an installation, a mixture of frying oils collected from different users, mainly from restaurants cooking fried potatoes, has been treated. This oil is 10 in the form of a viscous product, of very dark brown colour and exhaling a characteristic sickening odour such as may be encountered in certain poorly ventilated restaurant kitchens.

Its composition is not known precisely, but it is constituted by a mixture of fats of vegetable origin: sunflower, rape-seed and peanut oils and partially 15 hydrogenated palm oil. In order to render it easy to pump, it was disposed in a recipient heated to 60°C. It was then injected by the pump 5 into the installation described previously and was mixed in the mixer 1 with a flow of fluid at supercritical pressure constituted by carbon dioxide furnished by the pump 5, with an addition of a co-solvent constituted by ethanol furnished by pump 11 20 under the following conditions:

- flowrate of frying oil to be treated: 4 kg/hr.
- flowrate of carbon dioxide: 41.3 kg/hr.
- flowrate of ethanol: 3 kg/hr.
- Pressure in the mixer 1 and the separator 3: 25 MPa
- 5 - Temperature in the mixer 1 and the separator 3: 50°C
- Pressure in the separators 19, 21, 23 after expansion of the fluid: 4.5 MPa

Under these conditions, an extract is obtained at the outlet of the lock

chambers 25, 27, 29, which, after elimination of the ethanol entrained in a rotary evaporator in vacuo, is in the form of a yellow-orange oil, limpid and virtually odour-free.

On the contrary, the residue is in the form of a dark brown viscous liquid with an odour even more sickening than that of the initial oil. Over a period of two hours, 8 kg of used oil were injected and 2.8 kg of refined oil and 5.2 kg of residue were collected.

15 EXAMPLE 2: Treatment of a used frying oil in a mixer-decanter with partial recycling of the residue:

The procedure is the same as in the case of the preceding Example. However, the temperature in the mixer 1 is taken to 70°C and it is no longer the crude used oil alone which is treated, but about 96% of the residue is recycled, 20 the flowrate of the injected oil being taken to 28 kg/hr.

Under these conditions, the extract obtained after elimination of the ethanol is in the form of an oil which is slightly more orange-coloured than the one obtained previously,

but still limpid and virtually odourless. The appearance of the residue is similar to that obtained earlier. Over a period of eight hours, 18 kg of used oil were treated and 10.4 kg of refined oil and 7.6 kg of residue were collected.

It will therefore be understood that the partial recycling of the residue  
5 allows a substantial increase in the final yield of extraction of the refined oil with respect to the initial oil, which therefore attains 58% instead of 35% in the case described in the preceding Example.

## CLAIMS

1. Method for fractionating a cooking oil, in particular frying oil, using a solvent at supercritical pressure, characterized in that it comprises the steps  
5 consisting in:

- contacting, in a mixer, the cooking oil with the solvent at supercritical pressure;

- separating the resulting mixture into two phases in a decanter, namely a light phase and heavy phase;

10 - decompressing the light phase and the heavy phase so as to recuperate the solvent and the treated oil and the treatment residues respectively.

2. Method according to Claim 1, characterized in that the fluid at supercritical pressure is constituted by carbon dioxide.

3. Method according to Claim 2, characterized in that the fluid at supercritical pressure is constituted by a mixture of an organic solvent in carbon dioxide at a pressure included between 7.4 MPa and 50 Mpa, and more favourably between 20 MPa and 40 MPa and at a temperature included between 0°C and 80°C.

4. Method according to Claim 3, characterized in that the solvent is a light hydrocarbon having between 2 and 5 carbon atoms, such as ethane, propane and butane.

20 5. Method according to Claim 3, characterized in that the solvent is an alcohol, and more favourably ethanol.

6. Method according to Claim 3, characterized in that the solvent is a ketone, and more favourably acetone.

7. Method according to Claim 3, characterized in that the solvent is an ester, and more favourably ethyl acetate.

5 8. Method according to any one of the preceding Claims, characterized in that the heavy phase is recycled in part with the initial feedstock constituted by the cooking oil to be treated.

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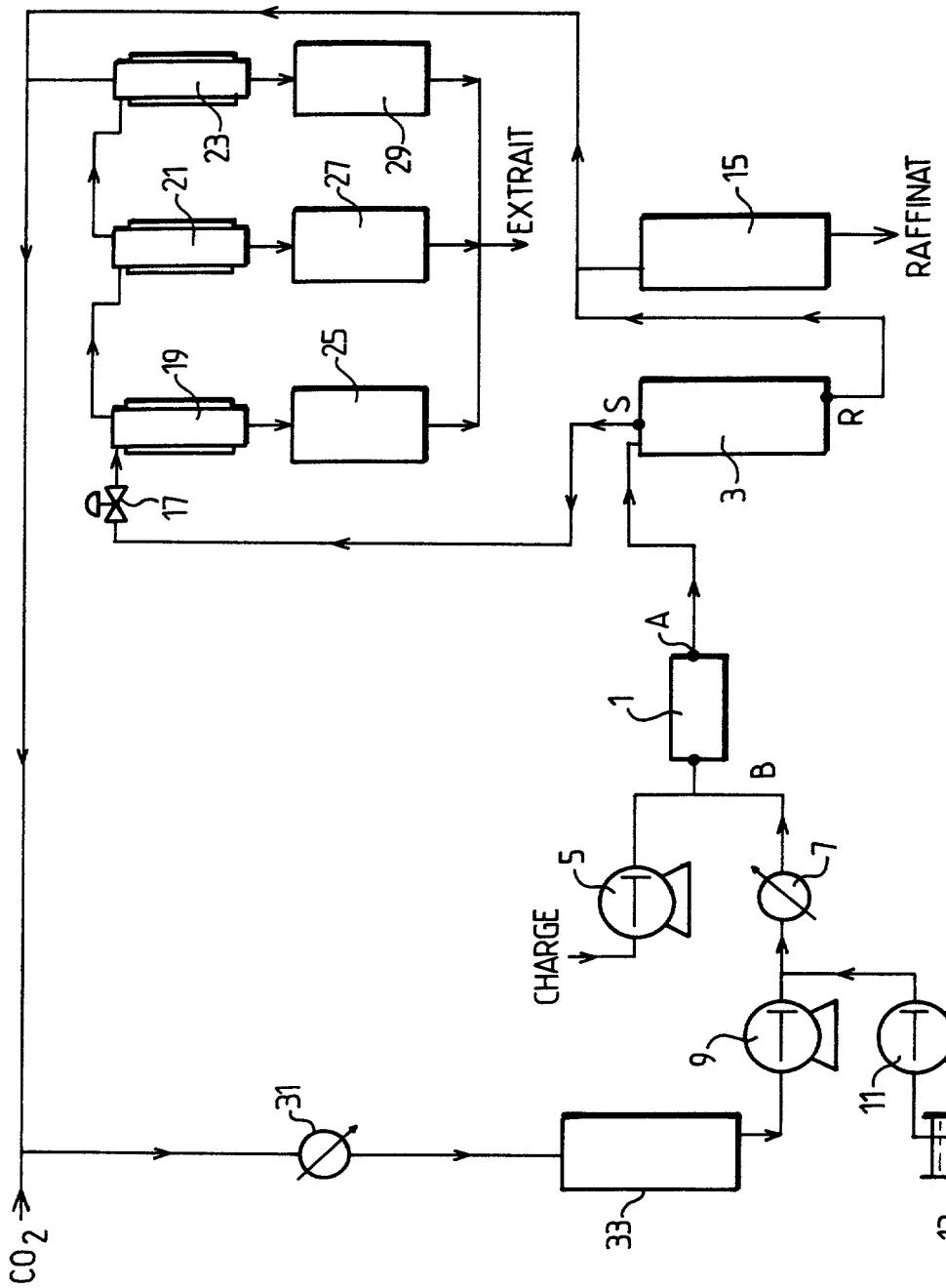


FIG. UNIQUE

**DECLARATION FOR UTILITY OR  
DESIGN  
PATENT APPLICATION  
(37 CFR 1.63)**

Declaration Submitted with Initial Filing

OR

Declaration Submitted after Initial Filing (surcharge (37 CFR 1.16 (e)) required)

Attorney Docket Number	366325-520
First Named Inventor	Perrut, Michel
<b>COMPLETE IF KNOWN</b>	
Application Number	/
Filing Date	
Art Unit	
Examiner Name	

As the below named inventor, I hereby declare that:

My residence, mailing address, and citizenship are as stated below next to my name.

I believe I am the original and first inventor of the subject matter which is claimed and for which a patent is sought on the invention entitled:

**METHOD FOR FRACTIONATING COOKING OIL**

*(Title of the Invention)*

the specification of which

is attached hereto

OR

was filed on (MM/DD/YYYY) [redacted]

as United States Application Number or PCT International

Application Number [redacted] and was amended on (MM/DD/YYYY) [redacted] (if applicable).

I hereby state that I have reviewed and understand the contents of the above identified specification, including the claims, as amended by any amendment specifically referred to above.

I acknowledge the duty to disclose information which is material to patentability as defined in 37 CFR 1.56, including for continuation-in-part applications, material information which became available between the filing date of the prior application and the national or PCT international filing date of the continuation-in-part application.

I hereby claim foreign priority benefits under 35 U.S.C. 119(a)-(d) or (f), or 365(b) of any foreign application(s) for patent, inventor's or plant breeder's rights certificate(s), or 365(a) of any PCT international application which designated at least one country other than the United States of America, listed below and have also identified below, by checking the box, any foreign application for patent, inventor's or plant breeder's rights certificate(s), or any PCT international application having a filing date before that of the application on which priority is claimed.

Prior Foreign Application Number(s)	Country	Foreign Filing Date (MM/DD/YYYY)	Priority Not Claimed	Certified Copy Attached?	
				YES	NO
99/07728	FR	06/18/1999	<input type="checkbox"/> <input type="checkbox"/> <input type="checkbox"/>	<input type="checkbox"/> <input type="checkbox"/> <input type="checkbox"/>	<input checked="" type="checkbox"/> <input type="checkbox"/> <input type="checkbox"/>

Additional foreign application numbers are listed on a supplemental priority data sheet PTO/SB/02B attached hereto:

[Page 1 of 2]

PTO/SB/01 (1-01)  
Approved for use through 10/31/2002. OMB 0651-0032

U.S. Patent and Trademark Office; U.S. DEPARTMENT OF COMMERCE

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**DECLARATION — Utility or Design Patent Application**

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or Bar Code Label **25561** OR  Correspondence address below

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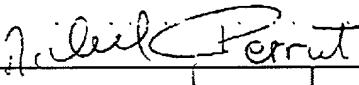
Telephone \_\_\_\_\_

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I hereby declare that all statements made herein of my own knowledge are true and that all statements made on information and belief are believed to be true; and further that these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under 18 U.S.C. 1001 and that such willful false statements may jeopardize the validity of the application or any patent issued thereon.

**NAME OF SOLE OR FIRST INVENTOR:**  A petition has been filed for this unsigned inventor

Given Name (first and middle [if any])	<u>Michel</u>	Family Name or Surname	<u>Perrut</u>
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Inventor's Signature		Date	<u>12/12/01</u>
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City	<u>54000 Nancy</u>	State	<u>France</u>	Country	<u>France</u>
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**NAME OF SECOND INVENTOR:**  A petition has been filed for this unsigned inventor

Given Name (first and middle [if any])	<u>Wieslaw</u>	Family Name or Surname	<u>Majewski</u>
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Inventor's Signature		Date	<u>13/12/01</u>
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Residence: City	<u>Laxou</u>	State	<u>France</u>	Citizenship	<u>French</u>
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Additional inventors are being named on the \_\_\_\_\_ supplemental Additional Inventor(s) sheet(s) PTO/SB/02A attached hereto.

Please type a plus sign (+) inside this box → 

PTO/SB/01 (02-01)

Approved for use through 10/31/2002, OMB 0651-0035

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Application Number	Not Yet Assigned
Filing Date	Filed Herewith
First Named Inventor	Perrut
Title	Method for Fractionating .....
Group Art Unit	Not Yet Assigned
Examiner Name	Not Yet Assigned
Attorney Docket Number	366325-520

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Statement under 37 CFR 3.73(b) is enclosed: (Form PTO/SB/56).

**SIGNATURE of Applicant or Assignee of Record**

Name Michel Perrut

Signature



Date

12/12/2001

NOTE: Signatures of all the inventors or assignees of record of the entire interest or their representative(s) are required. Submit multiple forms if more than one signature is required; see below.

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